



A high-performance intermediate-temperature aluminum-ion battery based on molten salt electrolyte

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ABSTRACT

Non-aqueous rechargeable aluminum-ion batteries (AIBs) are a promising candidate for grid-scale energy storage due to their high theoretical energy density, safety, environmental benignity, and the abundance of Al sources. However, the limited cathode capacity and the high price of ionic liquid electrolytes hinder their large-scale applications. Herein, an intermediate-temperature AIB composed of nickel disulfide-based cathode and NaCl-AlCl₃-Al₂S₃ molten salt electrolyte is reported. A highly reversible conversion mechanism between Ni₃S₄ and Ni during cycling is proved with cathode capacities exceeding 500 mAh g⁻¹. The full cell delivers a cathode capacity of 320 mAh g⁻¹ at 240 °C and a current density of 2000 mA g⁻¹ with negligible capacity fade after 2000 cycles. The raw material cost is estimated to be as low as 28 \$ kWh⁻¹ based on the electrode and electrolyte materials. The molten salt electrolyte-based AIB provides promising opportunities to build energy storage systems with low cost, high safety, stable electrochemical performance, and long lifetime.

1. Introduction

Grid-scale energy storage is critical for renewable energy integration, and there is a desire to develop new electrochemical energy storage systems with high safety, low cost, and competitive energy density to fit the increasing requirements of large-scale applications [1]. In the past decades, lithium-ion batteries have achieved enormous success in energy storage applications [2]. However, researchers have to seek more sustainable battery systems considering the high cost, safety concerns, and recycling problems of lithium-based batteries [3,4]. In this regard, batteries based on sodium, magnesium, and aluminum have attracted much attention [5–8]. Among them, aluminum-ion batteries (AIBs) possess the potential to achieve high energy density and low energy cost due to the competitive specific capacity (2978 mAh g⁻¹) and low price (~2.6 \$ kg⁻¹) of aluminum [9]. Additionally, the high stability and safety of the metallic aluminum electrode make it much more preferable for battery manufacturing than the metallic lithium electrode [10].

AIBs can be classified into aqueous and non-aqueous systems based on the compositions of the electrolyte [11]. Aqueous electrolytes own lower cost and higher ionic conductivity but are limited by the narrow

electrochemical stability window [12,13]. Recently, significant progress has been made with respect to non-aqueous AIBs with room-temperature ionic liquid (IL) electrolytes and carbon-based cathodes [8,14–16]. Although the battery system demonstrates good rate performance and cycling stability, the high cost of IL electrolytes and the relatively low capacity of carbon-based cathodes challenge their practical applications [17]. As a result, metal sulfides such as nickel sulfides [18,19], molybdenum sulfides [20,21], cobalt sulfides [22,23], and vanadium sulfides [24,25], have been investigated as alternative cathode materials because of their potential to achieve higher capacities [26,27]. However, there is a large disparity between the cell-level capacities and their theoretical values due to the poor conductivity and the structural instability of such materials [17,28]. Moreover, the cathodes are synthesized at the nanoscale level with limited active material loadings of less than 3 mg cm⁻² in most cases [19–23,29–30]. Further research on cost-effective electrode synthesis routes suitable for mass production is required before real applications.

Herein, we report an intermediate-temperature aluminum-nickel disulfide battery (Al/NiS₂ battery) with molten salt electrolyte. The NiS₂@carbon black (NiS₂@C) cathode is prepared by an in-situ molten salt synthesis method with an ultrahigh active material loading of 30 mg

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cm^{-2} . Taking advantage of the high ionic conductivity of the $\text{NaCl-AlCl}_3\text{-Al}_2\text{S}_3$ electrolyte ($\sim 0.39 \text{ S cm}^{-1}$ at 180°C , comparable to $\sim 0.02 \text{ S cm}^{-1}$ for $\text{AlCl}_3\text{-[EMIm]Cl}$ at room temperature) [31,32], as well as the fast reaction kinetics at elevated temperatures [33], a superior cathode capacity of over 500 mAh g^{-1} is obtained. The Al/NiS_2 battery system presents excellent cycling stability and rate capability in a relatively wide working temperature window, delivering a cathode capacity of 380 mAh g^{-1} after 1000 cycles at 180°C and a current density of 1000 mA g^{-1} and a cathode capacity of 320 mAh g^{-1} after 2000 cycles at 240°C and a current density of 2000 mA g^{-1} . Meanwhile, the cell can tolerate repeated overcharges and recover after being cooled down to ambient temperature, ensuring stable operations with easy maintenance in practical application environments.

2. Material and methods

2.1. Materials

NaCl , AlCl_3 , S , NiCl_2 , Al , polytetrafluoroethylene (PTFE) preparation (60 wt% dispersion in H_2O), and alcohol used in this work were analytical reagent grade and commercially available from Aladdin Bio-Chem Technology Co., Ltd (Shanghai, China). Carbon black was purchased from Hefei Kejing Co., Ltd (Hefei, China). All chemicals were used directly without any purification. Glass microfiber filters (Whatman 934-AH) were used as separators.

2.2. Preparation of the $\text{NaCl-AlCl}_3\text{-Al}_2\text{S}_3$ electrolyte and the NaCl-AlCl_3 electrolyte

The $\text{NaCl-AlCl}_3\text{-Al}_2\text{S}_3$ electrolyte was prepared in an argon-filled glove box (Etelux, Lab2000). NaCl , AlCl_3 , and S powders were fully mixed with a molar ratio of 1.05:1.0:0.12. The mixture was heated with excess aluminum to 120°C for 10 h and 200°C for 72 h. The NaCl-AlCl_3 electrolyte was prepared in the same glove box. NaCl and AlCl_3 were fully mixed with a molar ratio of 1.05:1.0. The mixture was heated with excess aluminum to 120°C for 10 h and 200°C for 24 h. Both melts were clear and colorless, with extra NaCl precipitating at the bottom of the container. The transparent upper melts were poured out carefully and collected.

2.3. Preparation of the $\text{NiS}_2\text{@C}$ cathode and the $\text{NiCl}_2\text{@C}$ cathode

The $\text{NiS}_2\text{@C}$ cathode was prepared in three steps. Firstly, NiCl_2 was dissolved in an alcohol solution. Carbon black was impregnated with the solution and dried in an 80°C oven. Secondly, the as-prepared $\text{NiCl}_2\text{@C}$ was mixed with S and PTFE and processed into a thin slice as the cathode precursor. The cathode precursor was then pressed into two molybdenum meshes with a pressure of 30 MPa [34]. Thirdly, the cathode precursor was heated with the $\text{NaCl-AlCl}_3\text{-Al}_2\text{S}_3$ molten salt electrolyte at 180°C for 4 h to be transformed into the $\text{NiS}_2\text{@C}$ cathode through an in-situ molten salt synthesis method. The weight ratio of the applied NiCl_2 , C , S , and PTFE was 3:1:2:0.5, and it can be calculated that the weight ratio of the NiS_2 , C , and PTFE in the $\text{NiS}_2\text{@C}$ cathode was around 2.8:1:0.5. The active material loading was around 30 mg cm^{-2} . The $\text{NiCl}_2\text{@C}$ cathode was prepared in two steps. Firstly, NiCl_2 was dissolved in an alcohol solution. Carbon black was impregnated with the solution and dried in an 80°C oven. Secondly, the as-prepared $\text{NiCl}_2\text{@C}$ was mixed with PTFE , processed into a thin slice with a pressure of 30 MPa, and pressed into two molybdenum meshes. The weight ratio of the applied NiCl_2 , C , and PTFE was 3:1:0.5. The active material loading was around 30 mg cm^{-2} .

2.4. Assembly of the Al/NiS_2 battery and the Al/NiCl_2 battery

The Al/NiS_2 battery was assembled in three steps. Firstly, glass seals were applied between the Ta wire and the stainless-steel battery case.

The silicate-based glass has a melting point of 500°C and was heated to 750°C for 1 h in a muffle furnace (MTI) to reach the encapsulation. Secondly, the $\text{NaCl-AlCl}_3\text{-Al}_2\text{S}_3$ electrolyte (1.2 g) was filled in the Al case (1 mm thickness, $\sim 1.5 \text{ g}$) and was heated to 180°C . The Mo meshes were welded to the Ta wire, and the cathode ($\sim 1 \text{ cm}^2$, with active material loading of $\sim 30 \text{ mg}$) was immersed into the electrolyte. The first two steps were performed in the argon-filled glove box. Finally, the battery was cooled to ambient temperature and taken out to ambient air. Laser welding was quickly applied at the threaded connection to ensure airtightness. The assembly procedures of the Al/NiCl_2 battery were similar to that of the Al/NiS_2 battery, except that $\text{NiCl}_2\text{@C}$ was applied as the cathode.

2.5. Characterization technique

The microstructures of the samples were analyzed by scanning electron microscopy (MERLIN Compact Zeiss). Phase identifications of the samples were analyzed using X-ray diffraction (D-Max-2500 Rigaku XRD Analyzer) and X-ray photoelectron spectroscopy with a 300 W $\text{Al K}\alpha$ radiation (Amicus Budget). Raman spectra were obtained using a 532 nm laser (LabRAM HR Evolution). Element content analyses of the samples were conducted using inductively coupled plasma optical emission spectroscopy (Agilent 725 ICP-OES).

2.6. Electrochemical measurement

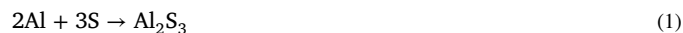
Assembled Al/NiS_2 batteries were tested in muffle furnaces (MTI) in ambient air. Battery performance was tested using a battery test system (LAND, 2001CT). Cyclic voltammetry measurements were conducted on an electrochemical workstation (CHI 660e) in two-electrode mode. Impedance measurements of assembled batteries were performed using a potentiostat with a frequency response analyzer (FRA) module (Metrohm Autolab).

3. Results

3.1. Battery structural and material design

Fig. 1a schematically demonstrates the Al/NiS_2 battery configuration, with a digital photo of an assembled cell shown in Fig. 1b. The Al case anode is filled with the $\text{NaCl-AlCl}_3\text{-Al}_2\text{S}_3$ molten salt electrolyte. The stainless-steel cylinder outside the anode serves as the current collector. $\text{NiS}_2\text{@C}$ cathode is pressed into molybdenum (Mo) meshes welded to a tantalum (Ta) wire. In order to prevent short circuits, a glass fiber separator is covered on the cathode. Glass seals are applied between the cathode and anode current collector for gas tightness and electronic insulation.

According to the relevant research, the ionic conductivity of the electrolyte increases while the vapor pressure decreases with the fraction of NaCl [31]. As a result, the composition with saturated NaCl was chosen, and the working temperature of the battery system is suggested to be above 180°C (Fig. S1). The ionic conductivity of the electrolyte was tested to be 0.39 S cm^{-1} at 180°C and increased with the elevated temperature (Fig. S2). It is noteworthy that sulfur was reported to react with aluminum and NaCl-AlCl_3 melts according to Eqs. (1) and (2) and exist in the form of chain species $[\text{AlSCl}_2]_n^{n-}$ in the molten state. “ NaAlSCl_2 ” is commonly used as an apparent formula [35,36].



The X-ray diffraction (XRD) pattern of the electrolyte at ambient temperature is shown in Fig. S3, and the peaks of NaAlCl_4 and Al_2S_3 were observed. The element contents of the electrolyte determined by inductively coupled plasma optical emission spectroscopy (ICP-OES) are listed

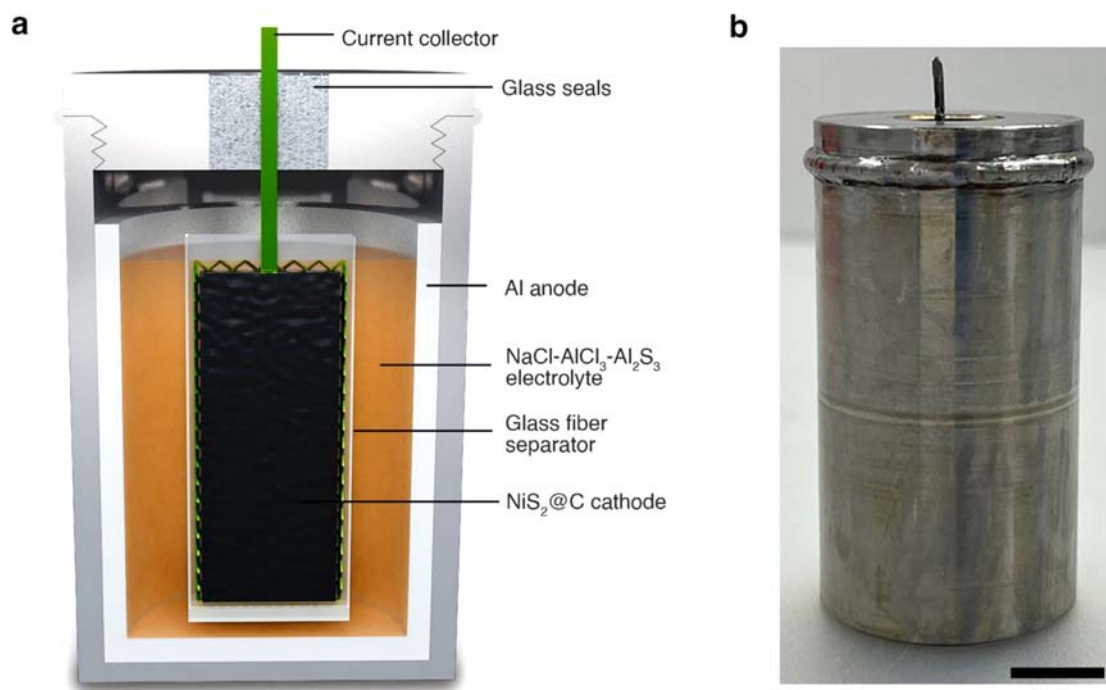
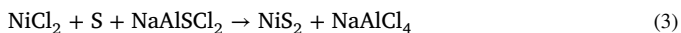


Fig. 1. Structural design of the Al/NiS₂ battery. (a) Schematic diagram of the Al/NiS₂ battery. (b) Digital photo of an assembled Al/NiS₂ battery. The scale bar is 1 cm.

in Table S1. It can be calculated that the molar ratio of NaCl, AlCl₃, Al₂S₃ was 1:1.03:0.03, which is reasonably consistent with the expected composition. The content of Al₂S₃ was slightly lower than expected, and it can be attributed to the H₂S volatilization through the hydrolysis reaction of Al₂S₃ during testing.

The NiS₂@C cathode was synthesized through an in-situ molten salt synthesis method. Firstly, NiCl₂ impregnated conductive carbon black (NiCl₂@C) was prepared. The NiCl₂@C powder was mixed with S powder and polytetrafluoroethylene (PTFE) binder and then processed into a thin slice as the cathode precursor (Fig. S4). The precursor was heated with the NaCl-AlCl₃-Al₂S₃ molten salt at 180 °C for 4 h and transformed into the NiS₂@C cathode through the following reaction.

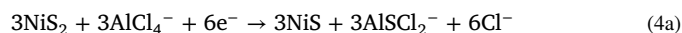


The scanning electron microscopy (SEM) images and the energy-dispersive X-ray (EDX) spectrum of the cathode precursor before and after being washed by deionized water are shown in Fig. 2a–2d. As seen in Fig. 2a and 2b, the surface of the precursor was covered by NiCl₂ with rod-like morphologies. After removing the NiCl₂ with deionized water, it was observed that a porous network was formed by carbon black with sulfur distributed evenly, ensuring high electrode conductivity and adequate electrolyte infiltration (Fig. 2c and 2d). The NiS₂@C cathode was also washed by deionized water to remove the electrolyte before a series of characterizations. The formation of NiS₂ was confirmed based on the XRD result in Fig. S5. SEM and the corresponding EDX spectrum (Fig. 2e and 2f) showed that the water-insoluble NiS₂ remained rod-like shapes with smaller diameters. X-ray photoelectron spectroscopy (XPS) spectra of the Ni 2p and S 2p are shown in Fig. 2g and 2h, respectively. Both the Ni 2p_{3/2} and the Ni 2p_{1/2} peaks were fitted into two spin-orbit doublets along with two satellite peaks at 861.5 and 879.0 eV. The peaks at 853.8 and 871.4 eV were attributed to Ni²⁺, while the peaks at 856.4 and 874.0 eV were attributed to Ni³⁺. The S 2p peak was simulated into two peaks located at 162.6 and 163.8 eV, which is consistent with the S 2p_{3/2} and S 2p_{1/2} orbitals. Meanwhile, the weak peak at 168.6 eV can be attributed to sulfur oxides on the sample surface [37]. Based on the

results above, the in-situ synthesis of the NiS₂@C cathode was realized and easily integrated into the battery assembly process.

3.2. Electrochemical process and mechanisms

After assembling, the Al/NiS₂ battery was cycled at an intermediate temperature of 180 °C and a current density of 100 mA g⁻¹ (all of the current densities of the Al/NiS₂ batteries are calculated based on the weight of NiS₂ used in cathodes). In the first discharge, three major voltage plateaus existed at 0.73 V, 0.55 V, and 0.33 V, respectively (Fig. 3a). In order to study the reaction mechanisms, three cathode samples (samples II–IV) were taken from the batteries at the end of each discharge plateau for XRD tests after being washed by deionized water to remove the electrolyte (Fig. 3b). As seen from the XRD pattern of sample II, the initial active substance NiS₂ was mostly transformed into α-NiS after the first discharge plateau. As the discharge process continued, peaks of Ni₃S₂ occurred in the XRD pattern of sample III. NiS and Ni₃S₄ were also confirmed to exist, which could be attributed to the incomplete reduction reactions. It is also worth noting that the remaining α-NiS, which is the Nickeline phase, experienced a crystal phase transformation to β-NiS, which is the Millerite phase. At the end of the first discharge, the nickel sulfide species were mainly reduced to metallic Ni. XPS tests were also conducted (Fig. S6a and Fig. S6b). The S 2p and Ni 2p peaks were nearly unchanged for samples I–III, demonstrating the existence of nickel sulfides [37–40]. The atomic ratio of S to Ni was reduced to around 1:8 for sample IV, which is consistent with the conclusion that metallic Ni served as the final discharge product. The peak at 856.1 eV can be attributed to the formation of NiO at the surface of the Ni grains [41]. Similar results were revealed by Raman spectra (Fig. S7a). The peak at 472 cm⁻¹ in the spectra of sample I and the peak at 285 cm⁻¹ in the spectrum of sample II corresponded to NiS₂ and NiS, respectively [42,43], while no peak was observed in the spectra of sample IV. Therefore, it can be concluded that the active substance, NiS₂, experienced multi-step reduction reactions in the first discharge as follows.



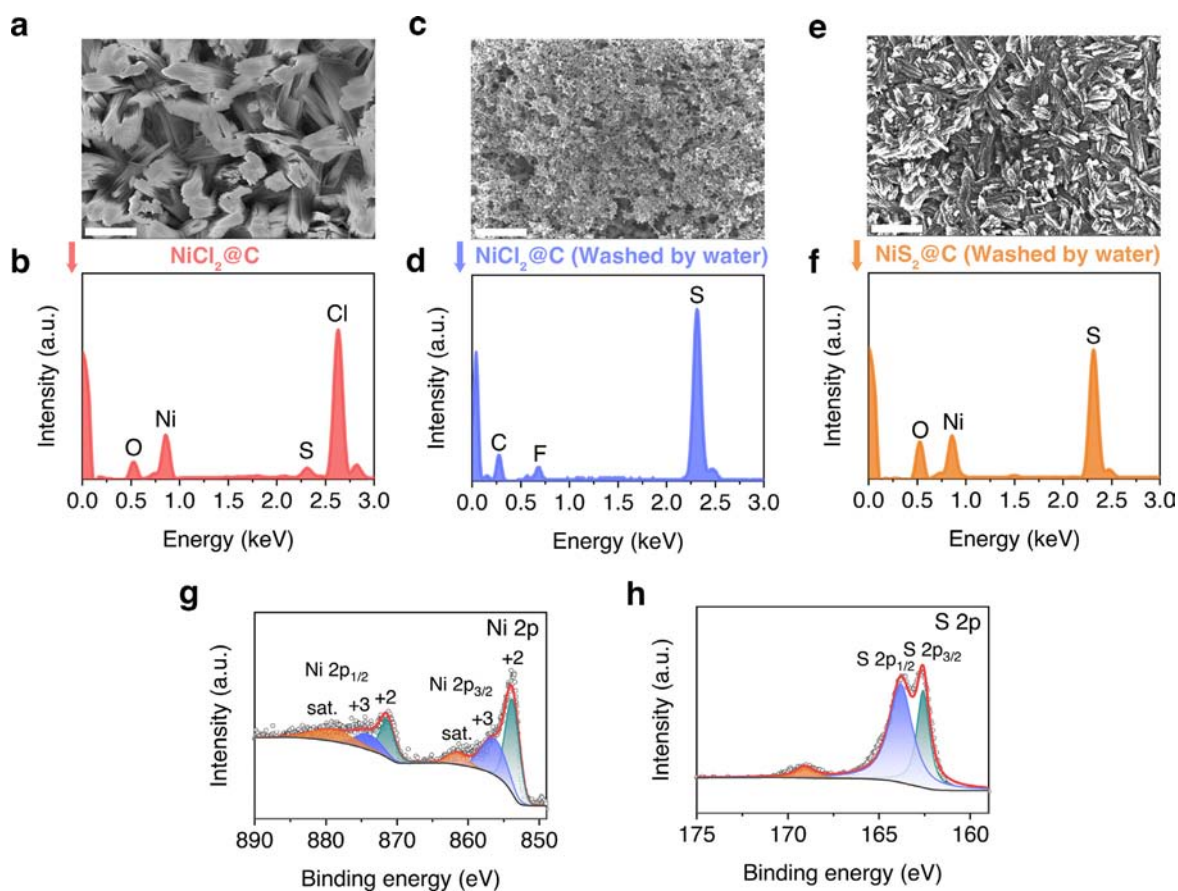
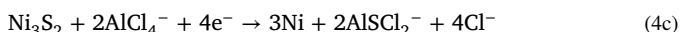
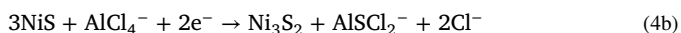


Fig. 2. Characterizations of the cathode precursor and the NiS₂@C cathode. (a) SEM image and (b) corresponding EDX spectrum of the cathode precursor. (c) SEM image and (d) corresponding EDX spectrum of the cathode precursor after being washed by deionized water. (e) SEM image and (f) corresponding EDX spectrum of the NiS₂@C cathode after being washed by deionized water. The scale bars are 2 μm. XPS spectra of (g) Ni 2p and (h) S 2p for the NiS₂@C cathode after being washed by deionized water.



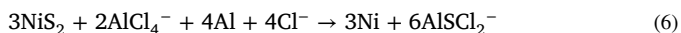
The full cell reactions in the first discharge can be formulated as:
Cathode:



Anode:



Overall:



It can be calculated from Fig. 3a that an initial discharging capacity of 840 mAh g⁻¹ was achieved (all of the specific capacities of the Al/NiS₂ batteries are calculated based on the weight of NiS₂ used in cathodes). The initial discharging capacity was close to the theoretical specific capacity of NiS₂ (878 mAh g⁻¹), indicating the high productivity of Eq. (3). Meanwhile, specific capacities of 410, 100, and 330 mAh g⁻¹ were obtained experimentally at each plateau, respectively, which was in good agreement with the theoretical capacity (439 mAh g⁻¹, 146 mAh g⁻¹, 293 mAh g⁻¹, respectively). The slight differences can be attributed to that part of the NiS was not reduced to Ni₃S₂ but directly transformed into metallic Ni, which was consistent with the XRD results.

Cyclic voltammograms (CV) were used to illustrate the electrochemical performance of the Al/NiS₂ battery after the first discharge. Fig. S8a presents the CV curves of the Mo meshes and Ta wire electrode (Mo/Ta electrode) and the NiS₂@C electrode at a slow scan rate of 0.1 mV s⁻¹ from 0 V to 1.5 V. Obvious anodic current signals were detected when the voltage reached 1.05 V in the CV curve of the Mo/Ta electrode, which indicated side reactions (detailed research will be discussed next). As a result, the battery was set to be cycled in the voltage range of 0–1.05 V, where no side reactions occurred (Fig. S8b and S8c). The CV curve of the NiS₂@C electrode presented three obvious oxidation peaks (0.80 V, 0.95 V, and 1.05 V) and three corresponding reduction peaks (0.27 V, 0.58 V, and 0.80 V), demonstrating multi-step reaction mechanisms [44].

The voltage profile of the first charge and the second discharge was also demonstrated in Fig. 3a. The three charge plateaus and three discharge plateaus were in good agreement with the CV curves. Six extra samples labeled from V-X were taken from the cathodes at the end of each voltage plateau and washed by deionized water. The reversibility of the cathode reactions was proved by the XRD tests (Fig. 3c). After the second discharge process, Ni was re-formed at the cathode. It is worth noting that NiS₂ was not detected in sample VII. Instead, Ni₃S₄ was the final charge product, with Ni₃S₂ and β-NiS serving as the intermediate substances. The above conclusions were verified by the XPS and Raman results (Fig. S6c, Fig. S6d, and Fig. S7b). The XPS and Raman spectra of the samples corresponding to the same state of charge/discharge (samples IV&X, samples V&IX, samples VI&VIII) were similar. It is also worth noting that the peak of NiS₂ was not observed in the Raman spectra of sample VII. Therefore, the cathode reactions after the first discharge can

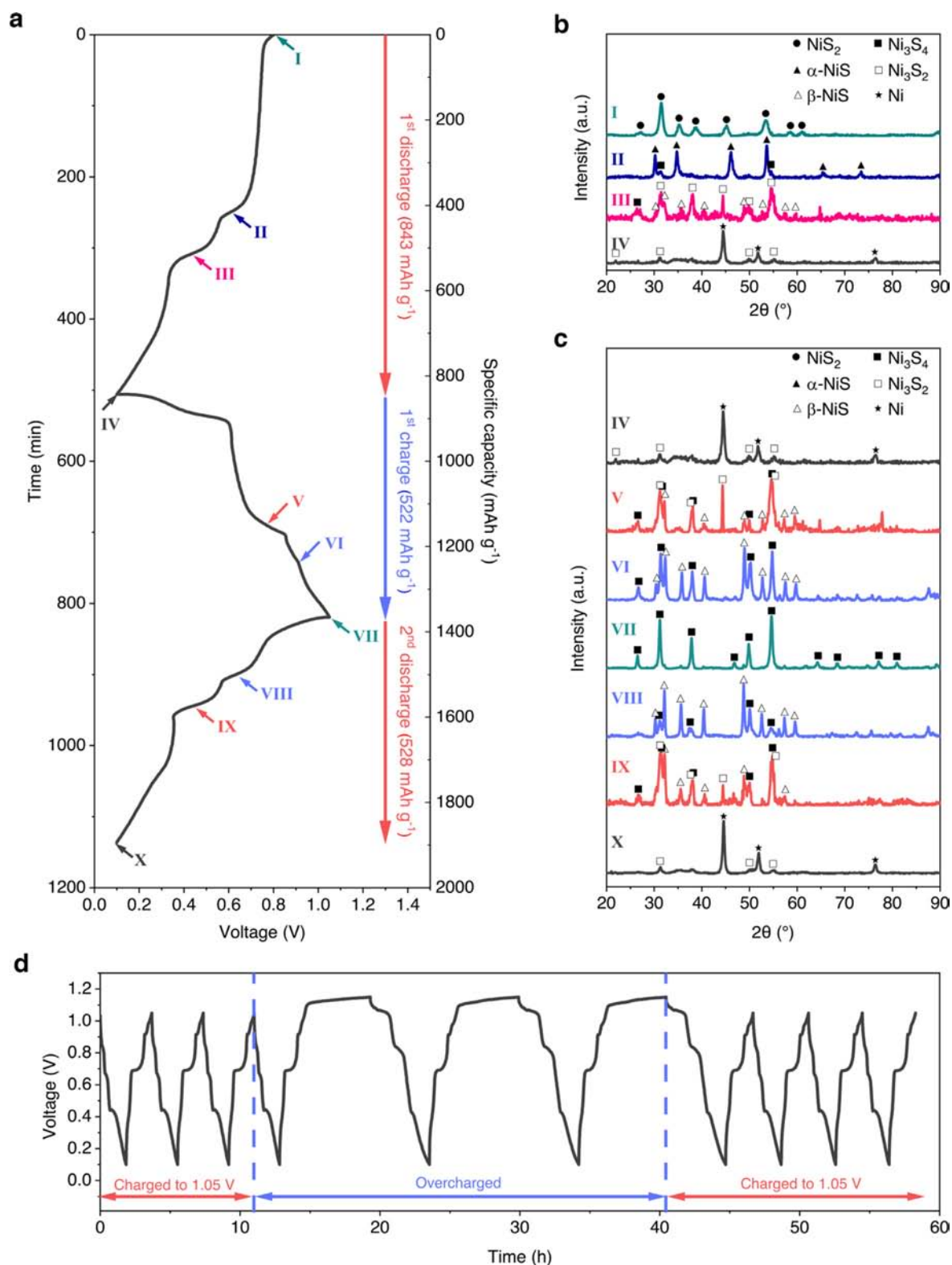


Fig. 3. Electrochemical process and reaction mechanisms of the Al/NiS₂ battery. (a) Voltage profile of the first cycle and the second discharge of the Al/NiS₂ battery cycled at 180 °C and a current density of 100 mA g⁻¹. Ten cathode samples were taken out from the batteries at different stages of charge/discharge and labeled as I to X, respectively. XRD patterns of the cathode samples (b) I-IV and (c) IV-X after being washed by deionized water. (d) Overcharge test of the Al/NiS₂ battery. The battery experienced three overcharged cycles during the cycling process. The current density was 250 mA g⁻¹.

be expressed as follows.



The full cell reactions after the first discharge can be formulated as:

Cathode:



Anode:



Overall:



Since Ni_3S_4 , instead of NiS_2 , served as the final charge product, the theoretical capacity related to the first discharge plateau in the second and the following cycles (135 mAh g^{-1}) was a third of that in the first cycle. Meanwhile, the discharging capacities related to the other two plateaus remained nearly unchanged because of the same reaction mechanisms.

Cathode samples I, IV, VII, X, and their corresponding anode samples (labeled as anode samples I, IV, VII, and X) were observed by SEM after being washed by deionized water. It can be seen in Fig. S9 that the active substances of the cathodes were distributed uniformly and adhered tightly to the carbon network. The final discharge product, Ni, showed similar spherical morphologies in cathode samples IV and X. Fig. S10 shows the morphology changes of the Al anode. Pores with diameters of 3–5 μm were formed on the anode surface after the first discharge, indicating the dissolution of Al. Part of the holes were filled in anode sample VII, which corresponded to the deposition process.

The reaction mechanisms and electrochemical stability of the cell during overcharges were further investigated. The Al/NiS₂ battery experienced three overcharged cycles at 180 °C and a current density of 250 mA g⁻¹ (Fig. 3d). A negligible capacity decay was observed after the battery was set back to cycle in the normal voltage range of 0–1.05 V. Fig. S11 shows the charge-discharge curve of an overcharged cycle and a normal cycle. An extra charge plateau existed at 1.09 V. Since Ta and Mo have been repeatedly reported to be electrochemically inert in the non-aqueous AIB systems [45–47], and sulfur was confirmed to be produced on the Mo/Ta electrode by the XRD test (Fig. S12), the corresponding reactions might be the oxidation of AlSCl_2^- ions to sulfur and other polymeric species [48]. The corresponding discharge plateau existed at 1.07 V with a much smaller capacity, mainly because the overcharge products were partly soluble in the electrolyte. It is also worth noting that the discharge plateau at 0.83 V in the overcharged cycle was longer than that in a normal cycle, reflecting changes in cathode reactions. A cathode sample was taken out from the overcharged battery for further investigations. After being washed by deionized water, the sample, labeled as cathode sample XI, was tested by XRD (Fig. S13). Peaks of NiS_2 and Ni_3S_4 were confirmed, which indicated that Ni_3S_4 was further oxidized during the overcharge process. To conclude, since both the electrolyte and the cathode experienced reversible oxidation reactions during the overcharge process, the cycling stability of the battery was not affected.

3.3. Battery performance

Charge-discharge measurements were performed in a voltage range of 0.1–1.05 V for further evaluation of the electrochemical performance of the Al/NiS₂ battery. Fig. S14 shows the charge-discharge curves of the 2nd, 4th, 6th, 8th, and 10th cycles at 180 °C and a current density of 250 mA g⁻¹. The discharging capacity in the 2nd cycle reached 520 mAh

g⁻¹, indicating around 90% usage of the active substances supposing Ni_3S_4 to be the final charge product. The voltage hysteresis experienced a noticeable decrease in the first six cycles, which can be attributed to a more uniform distribution of the active substances on carbon black during charge-discharge processes.

Fig. 4a shows the rate performance of the Al/NiS₂ battery at 180 °C, 210 °C, and 240 °C at various current densities ranging from 250 mA g⁻¹ to 2000 mA g⁻¹. The battery demonstrated extraordinary rate capability at all working temperatures. Even at a high current density of 2000 mA g⁻¹, the cathode delivered specific capacities of 310 mAh g⁻¹, 365 mAh g⁻¹, and 390 mAh g⁻¹ at 180 °C, 210 °C, and 240 °C, respectively. The charge-discharge curves at a current density of 250 mA g⁻¹ (Fig. 4b) show that decreased voltage hysteresis and increased specific capacities were achieved at elevated temperatures. Similar results were observed when batteries were cycled at different current densities (Fig. S15).

The Al/NiS₂ battery also demonstrated impressive cycling stability. A cathode capacity of 380 mAh g⁻¹ was achieved in the battery system cycled at 180 °C and a current density of 1000 mA g⁻¹ after 1000 cycles (Fig. 4c), while a cathode capacity of 320 mAh g⁻¹ was achieved in the battery system cycled at 240 °C and a current density of 2000 mA g⁻¹ after 2000 cycles (Fig. 4d). Both batteries demonstrated Coulombic efficiencies of nearly 100% and only showed slight capacity fade after the cycling.

The Al/NiS₂ battery showed prominent advantages in terms of cathode capacity, rate capability, and lifetime compared with other high-performance non-aqueous AIBs applying metal sulfide cathodes (Fig. 4e and 4f), which can be mainly attributed to three reasons [19,21,22,29,30,49–51]. Firstly, high electrolyte conductivity and fast reaction kinetics were achieved at high temperatures. Electrochemical impedance spectroscopy (EIS) was conducted, and the Nyquist plots of the Al/NiS₂ battery at different temperatures with the equivalent circuit are shown in Fig. S16. Small electrolyte resistance (1.43 Ω) and charge-transfer resistance (0.62 Ω) were achieved at 180 °C, and both values were further decreased with the temperature (Table S2). Secondly, the NiS₂@C cathode owns high structural stability during cycling. Metal sulfides are commonly synthesized on the nanoscale for room-temperature AIBs [24], which may lead to structural collapse and particle agglomeration. In contrast, the NiS₂@C cathode was prepared in a much simpler way with particle sizes on the micron scale. After being washed by deionized water, the cathode sample taken from the battery cycled at 180 °C for 1000 cycles was observed by SEM (Fig. S17). The active substances of the cathode remained in tight connections with the carbon conductive network, and no apparent grain growth was observed. The XRD results also demonstrated that the final charge and discharge products remained nearly unchanged after cycling, except some intermediate products were not fully involved in the reaction (Fig. S18 and Fig. S19). Thirdly, it has been reported that metal sulfide cathodes may experience decomposition and dissolution in chloroaluminate-based ILs [27,52,53]. However, the cathode materials at different states of charge/discharge were confirmed to be insoluble in the electrolyte (Table S3). It is worth noting that the results above also proved the necessity of synthesizing the sulfide cathode since NiCl_2 is partially soluble in NaCl-AlCl₃ melts (Table S4). A battery using NiCl_2 @C cathode and NaCl-saturated NaCl-AlCl₃ melts electrolyte was assembled for comparisons (Fig. S20). The initial cathode capacity was 410 mAh g⁻¹ based on the weight of NiCl_2 used in the cathode, which almost reached the theoretical value (416 mAh g⁻¹). However, the capacity decayed rapidly to 160 mAh g⁻¹ after 20 cycles.

As seen in Table S5, the intermediate-temperature Al/NiS₂ battery also demonstrated higher mass energy density (204 Wh kg⁻¹) and volumetric energy density (673 Wh L⁻¹) with lower raw material cost (28 \$ kWh⁻¹) comparable to AIBs with graphite cathodes (67 Wh kg⁻¹, 101 Wh L⁻¹, and 530 \$ kWh⁻¹). The Al/NiS₂ battery owns higher energy densities because of the high capacities of both the cathode and the anode. It is noteworthy that the Al/NiS₂ battery is assembled in the charged state, while the Al/AlCl₃-[EMIm]Cl/graphite

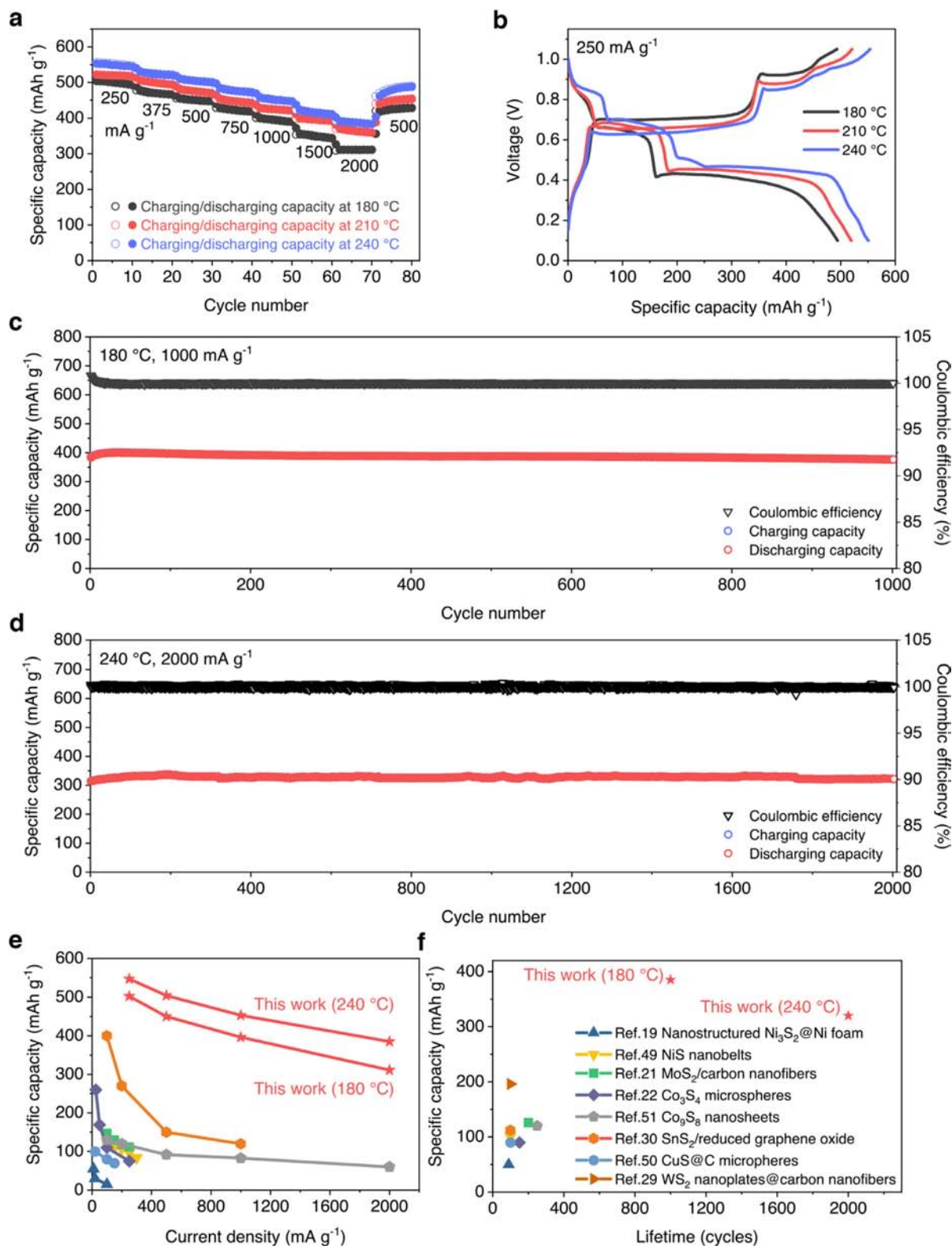


Fig. 4. Electrochemical performance of the Al/NiS₂ battery. (a) Specific capacities at different current densities ranging from 250 mA g⁻¹ to 2000 mA g⁻¹ at 180 °C, 210 °C, and 240 °C. (b) Charge-discharge curves at a current density of 250 mA g⁻¹ at 180 °C, 210 °C, and 240 °C. (c) Cycling performance over 1000 cycles at 180 °C and a current density of 1000 mA g⁻¹. (d) Cycling performance over 2000 cycles at 240 °C and a current density of 2000 mA g⁻¹. (e, f) Comparisons of the Al/NiS₂ battery with other high-performance non-aqueous AIBs applying metal sulfide cathodes in terms of cathode capacity, rate capability, and lifetime [19,21,22,29,30,49–51].

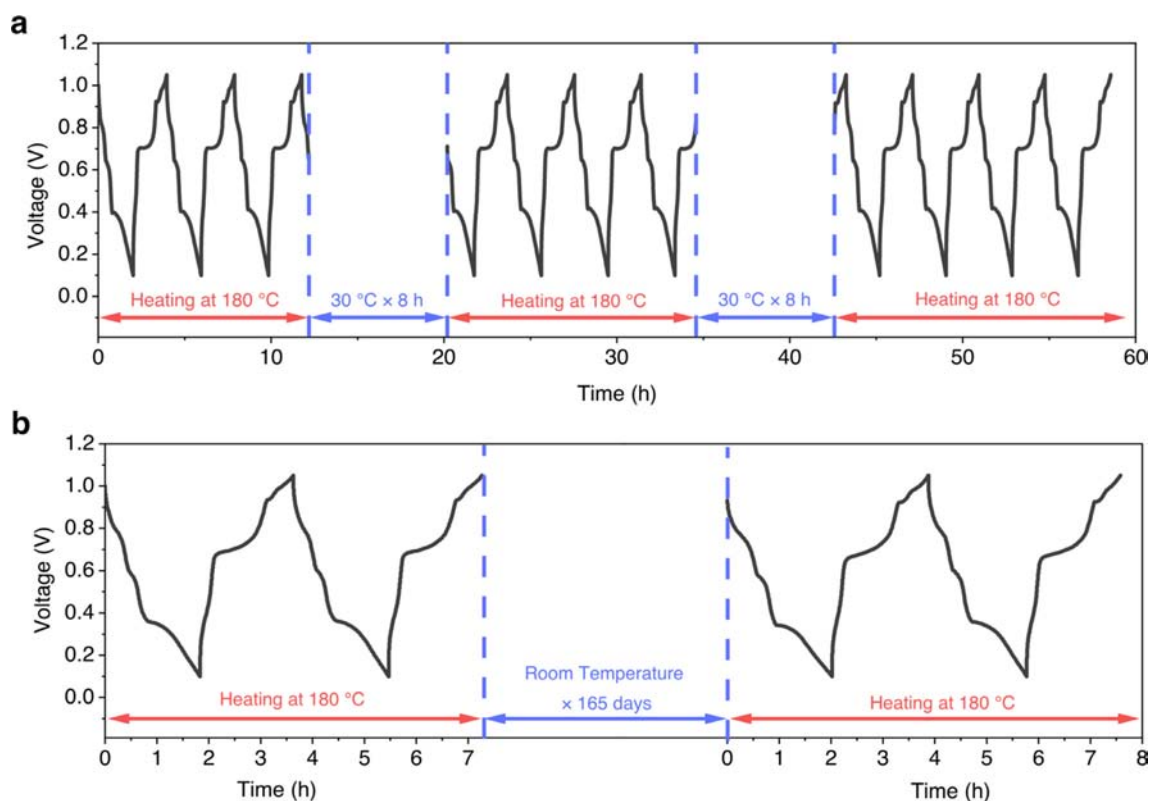


Fig. 5. Freezing-thawing tests of the Al/NiS₂ battery. (a) The battery was terminated and cooled down to 30 °C for 8 h during a charge and a discharge process. The current density was 250 mA g⁻¹. (b) After being charged to 1.05 V, the battery was terminated, cooled down, and kept at room temperature for 165 days. Then the battery was heated to 180 °C and restarted.

battery is assembled in the discharged state. For the former, NiS₂ (~550 mAh g⁻¹) serves as the cathode, metal Al (2978 mAh g⁻¹) serves as the anode, and the molten salt electrolyte is not the active substance in the electrochemical reactions. For the latter, graphite (~120 mAh g⁻¹) serves as the cathode, and AlCl₃ can be considered the actual anode material. As a result, a large amount of IL should be added, leading to low anode capacities (<46 mAh g⁻¹) [54–56]. Moreover, the raw material cost of Al/AlCl₃-[EMIm]Cl/graphite battery is much higher because of the application of the IL electrolyte (48.6 \$ kg⁻¹, comparable to 0.7 \$ kg⁻¹ for the inorganic molten salt electrolyte).

To conclude, the Al/NiS₂ battery demonstrated superior electrochemical performance with lower raw material cost over ambient-temperature non-aqueous Al-ion batteries. Compared with other high-temperature battery systems, the Al/NiS₂ battery can provide higher security because of the relatively low working temperature and the absence of molten alkali metals (Table S6) [57–59]. In addition, although the energy densities of the Al/NiS₂ battery are lower than those of the high-temperature Na/NiCl₂ battery and Li/ZnCl₂ battery systems, applying the molten salt electrolyte instead of ceramic electrolytes makes the battery system more suitable for large-scale applications [58,59].

Reliable and affordable electricity systems based on wind and solar may depend on the ability to store large quantities of low-cost energy over long timescales [60]. Although long-duration energy storage is urgently desired for the deployment of low-carbon grids in recent years, few technologies have succeeded at scale [61,62]. Our intermediate-temperature Al/NiS₂ battery, however, may be a promising candidate for long-duration energy storage for two reasons. Firstly, the material cost of the battery system is relatively low, which means the installed energy capital costs can be reduced to an acceptable level. Secondly, the battery can be kept at room temperature to avoid self-discharge and re-

duce maintenance costs. As seen in Fig. 5a, the battery was terminated and cooled down to 30 °C for 8 h during a charge and a discharge process. When the working temperature returned to 180 °C, the cell worked normally with no open nor short circuits, and no significant capacity decay was observed. Meanwhile, in Fig. 5b, after being charged to 1.05 V and kept at room temperature for over 5 months, the battery could be restarted and showed negligible self-discharge. Therefore, the battery system can be charged at working temperatures and store energy over long timescales without self-discharge at ambient temperature, which provides a new scheme for long-duration energy storage with low cost, high safety, and high reliability.

4. Conclusions

Our work develops an intermediate-temperature AIB based on the NiS₂@C cathode and the NaCl-AlCl₃-Al₂S₃ molten salt electrolyte. The multi-step conversion between Ni₃S₄ and Ni is clarified and applied as cathode reactions. The battery system shows broad prospects for large-scale applications. Firstly, applying the inorganic molten salt electrolyte instead of the IL electrolyte reduces the material cost, while applying the in-situ molten salt synthesis method for cathode preparation reduces the manufacturing cost. Secondly, the battery system has a competitive theoretical energy density of 204 Wh kg⁻¹ and 673 Wh L⁻¹. Experimentally, an ultrahigh cathode capacity of over 500 mAh g⁻¹ is obtained. The full cell also shows excellent overall performance. A cathode capacity of 320 mAh g⁻¹ is achieved in the battery cycled at 240 °C and a current density of 2000 mA g⁻¹ after 2000 cycles. Thirdly, the stability against overcharges and the ability to recover from frozen states of the battery system guarantee high robustness during operations. Overall, the low cost, high safety, and stable electrochemical performance of the Al/NiS₂ battery system make it a promising candidate for future concentrated and large-scale energy storage applications.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data Availability

The data that support the findings of this study are available from the corresponding author upon reasonable request.

CRedit authorship contribution statement

Kuangyu Wang: Conceptualization, Formal analysis, Investigation, Writing – original draft, Writing – review & editing. **Kai Liu:** Conceptualization, Formal analysis, Writing – original draft, Writing – review & editing. **Cheng Yang:** Investigation, Writing – original draft. **Ziyao Chen:** Investigation, Writing – original draft. **Haitian Zhang:** Investigation, Writing – original draft. **Yulong Wu:** Investigation, Writing – original draft. **Yuansheng Long:** Investigation, Writing – original draft. **Yang Jin:** Writing – original draft, Writing – review & editing. **Xiangming He:** Writing – original draft, Writing – review & editing. **Meicheng Li:** Writing – review & editing. **Hui Wu:** Conceptualization, Formal analysis, Writing – original draft, Writing – review & editing, Supervision, Project administration.

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Supplementary materials

Supplementary material associated with this article can be found, in the online version, at doi:10.1016/j.ensm.2022.03.030.

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